IN THE SPECIFICATION

Please replace the paragraph beginning at page 10, line 21, with the following rewritten paragraph:

Figure 2 is a schematic diagram of an apparatus for carrying out the second embodiment of the process according to the present invention. At the mixing site [[11]] 21, the chlorosilane-containing gas stream [[12]] 22 is introduced into the tubular reactor [[13]] 23, whose inner walls are wetted with "another aqueous liquid" [[22]] 32, such as tap water or deionized water. The walls of the tubular reactor [[13]] 23 are cooled by the cooling agent [[14]] 24. Upon entry into the tubular reactor [[13]] 23, the velocity of the gas stream [[12]] 22 decreases greatly. The treatment of the gas stream [[12]] 22 with the steam originating from the other aqueous liquid [[22]] 32 takes place in the tubular reactor [[13]] 23, with formation of hydrogen chloride and primary hydrolysis products. The formation of secondary hydrolysis products takes place in the other aqueous liquid [[22]] 32 which wets the wall of the equipment, resulting in a suspension. This suspension is separated from the purified gas stream [[16]] 26 in the collecting container [[15]] 25 and removed continuously or periodically as a hydrolyzate suspension [[15]]. The purified gas stream [[16]] 26 then passes through the scrubber [[17]] 27 which can be charged, for example with water, and leaves the system as waste gas [[18]] 28. Scrubber [[17]] 27 may also be used for monitoring the content of residual silicon-containing compounds in the gas stream. To re-use the other aqueous liquid [[22] 32, the suspension can be recycled as a stream [[19]] 29 until the concentration of the secondary hydrolysis products has reached a predetermined value. In addition, the circulation stream [[19]] 29 can be treated to neutralize the hydrogen chloride formed by the hydrolysis of chlorosilanes with an aqueous alkaline liquid [[21]] 31, which can be removed, for example, from the reservoir [[20]] 30. If the other aqueous liquid [[22] 32 or the circulation stream [[19]] 29 is rendered alkaline in this manner, largely soluble

silicon compounds result, thereby markedly reducing the tendency for deposits to form on tubular reactor [[13]] 23 and collecting container [[15]] 25.

Please replace the paragraph beginning at page 12, line 15, with the following rewritten paragraph:

Figure 3 is a schematic diagram of an apparatus for carrying out the third embodiment of the process of the present invention. At the mixing site [[31]] 41, the chlorosilane-containing gas stream [[32]] 42 and steam [[33]] 43 are introduced into the tubular reactor [[34]] 44, where the treatment of the chlorosilane-containing gas stream [[32]] 42 with steam [[33]] 43 takes place with formation of primary hydrolysis products. The tubular reactor [[34]] 44 dips into the cooling container [[35]] 45, whose inner walls are wetted with the "other aqueous liquid" [[44]] 54. In addition, the walls of tubular reactor [[34]] 44 can be cooled by means of a cooling agent [[36]] 46. The flow rate of gas streams [[32]] 42 and [[33]] 43 greatly decreases upon entry into the cooling container [[35]] 45. Steam [[33]] 43 condenses in the interior of the cooling container [[35]] 45, and the condensate is transported to the wetted equipment wall together with secondary hydrolysis products by means of a Stefan flow. The resulting suspension of secondary hydrolysis products, condensed steam [[33]] 43 and other aqueous liquid [[44]] 54 runs off the walls, is collected in the collecting container [[37]] 47 and removed continuously or periodically. The purified residual gas [[38]] 48 then passes through the scrubber [[39]] 49, which may be charged, for example, with water, and leaves the system as waste gas [[40]] 50. In addition, scrubber [[39]] 49 may be used to ~~monitoring~~ monitor the residual content of silicon-containing compounds in the gas stream. In the third embodiment of the process of the present invention, it is generally not necessary to remove hydrogen chloride from the waste gas [[40]] 50. In order to minimize use of the "other aqueous liquid" [[44]] 54, the suspension may be recycled as

stream [[41]] 51 until the concentration of the secondary hydrolysis products has reached a predetermined value. In addition, the circulation stream [[41]] 51 may be treated with an aqueous alkaline liquid [[43]] 53, for example, from the reservoir [[42]] 52, to neutralize the hydrogen chloride formed by hydrolysis of chlorosilanes. If the "other aqueous liquid" [[44]] 54 or the circulation stream [[41]] 51 is rendered alkaline in this manner, largely soluble silicon compounds result, thereby markedly reducing the tendency deposits to form on cooling containers [[35]] 45 and collecting container [[37]] 47.